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Supporting Information

Acetic Acid Ketonization over Fe₃O₄/SiO₂ for Pyrolysis Bio-Oil Upgrading

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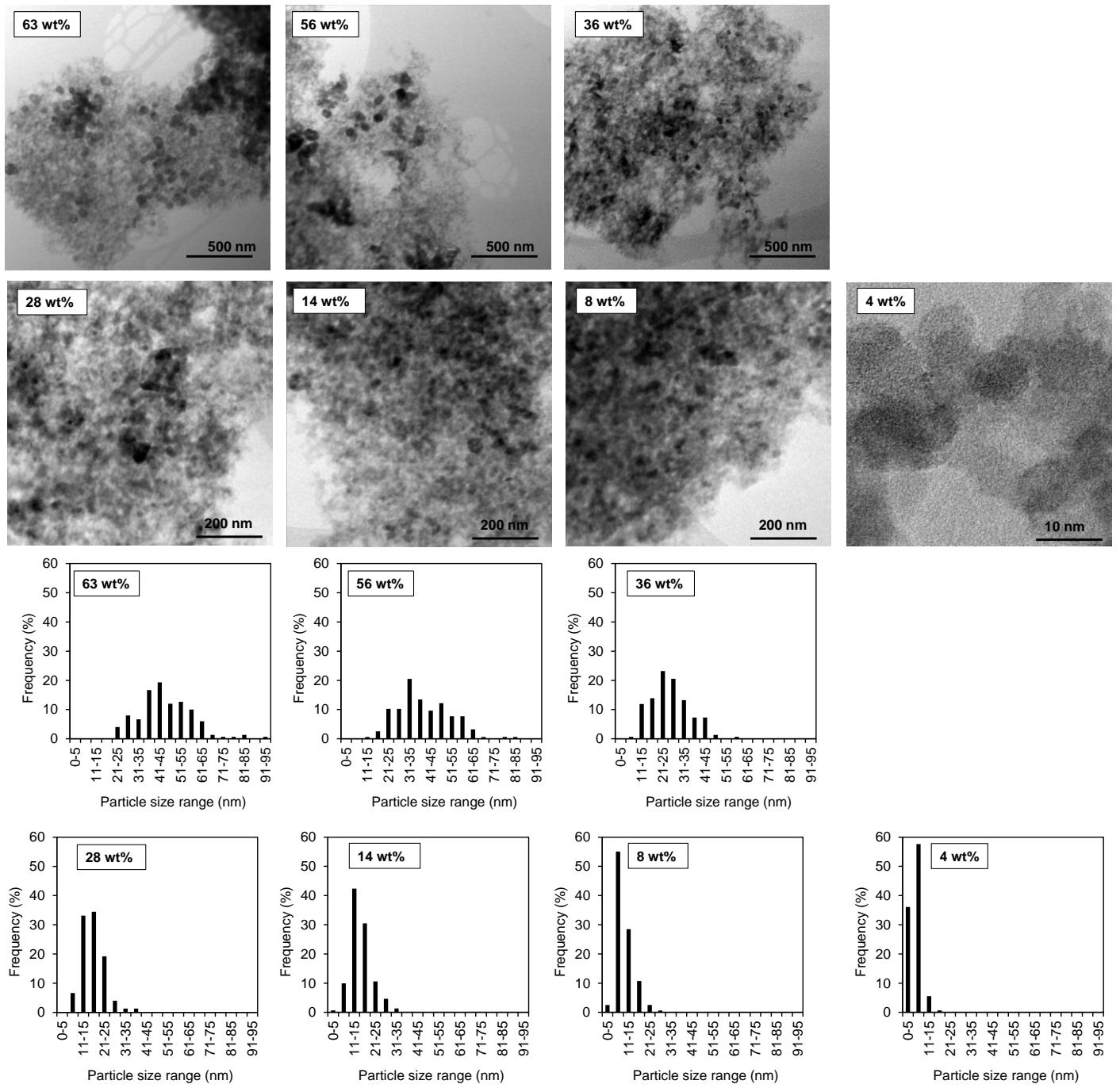


Figure S1. (top) Bright-field TEM images, and (bottom) particle size distributions for $\text{Fe}_3\text{O}_4/\text{SiO}_2$ catalysts.

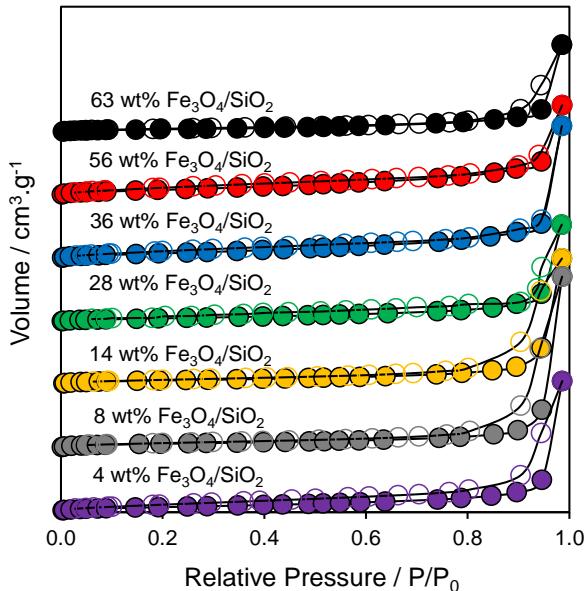


Figure S2. N_2 adsorption-desorption isotherms for $\text{Fe}_3\text{O}_4/\text{SiO}_2$ catalysts. Adsorption isotherms are represented by solid markers and desorption isotherms by hollow markers.

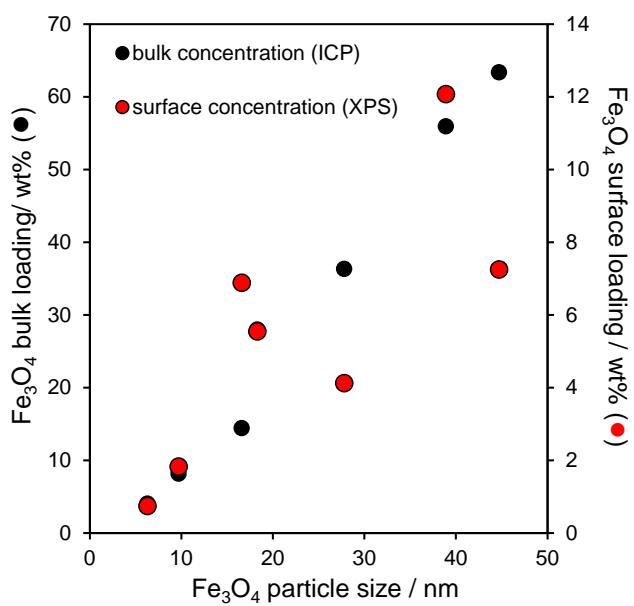


Figure S3. Surface and bulk Fe_3O_4 loadings as a function of particle size (determined by XRD) for $\text{Fe}_3\text{O}_4/\text{SiO}_2$ catalysts.

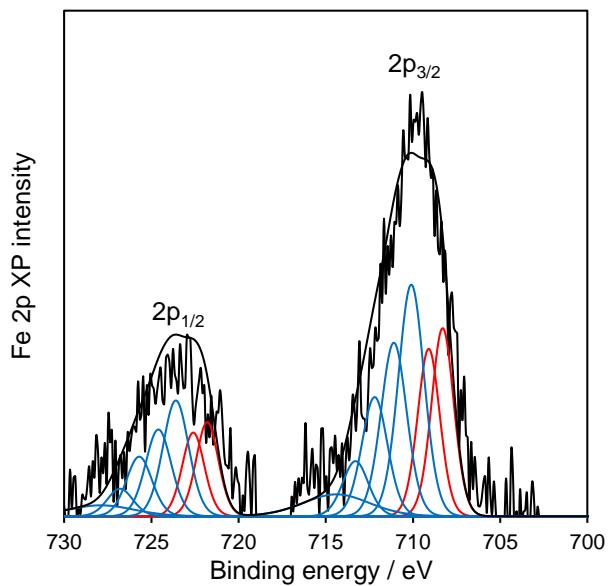


Figure S4. Fitted Fe 2p XP spectra for 63 wt% $\text{Fe}_3\text{O}_4/\text{SiO}_2$. Experimental data is shown in grey, fitted curve in black and Fe^{2+} and Fe^{3+} components in red and blue respectively.

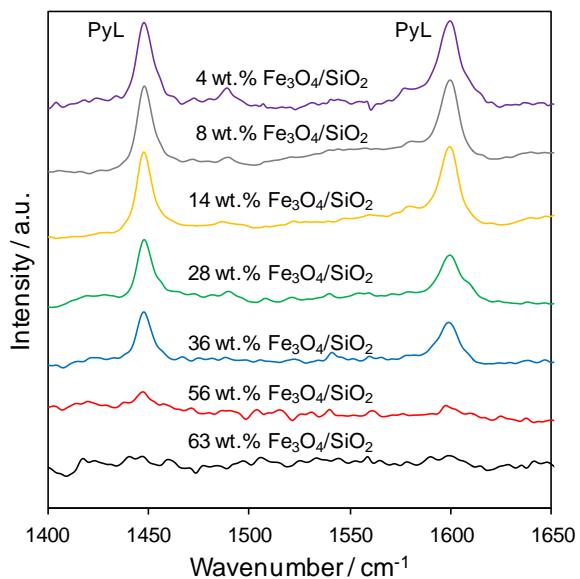


Figure. S5. DRIFT spectra of chemisorbed pyridine over $\text{Fe}_3\text{O}_4/\text{SiO}_2$ catalysts recorded at 50 °C in vacuo. Bands labelled PyL arise from pyridine adsorbed over Lewis acid sites.

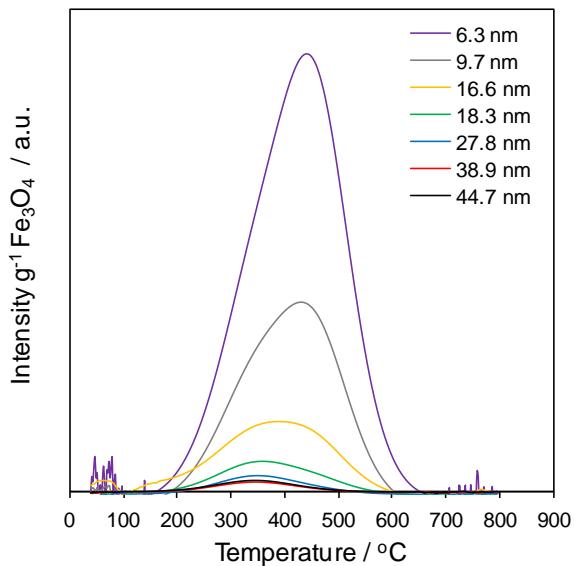


Figure S6. TPD of reactively-formed propene (m/z 41 channel) from chemisorbed propylamine normalised to the mass of Fe_3O_4 , and background subtracted to remove contributions from molecular propylamine adsorbed on the silica support.

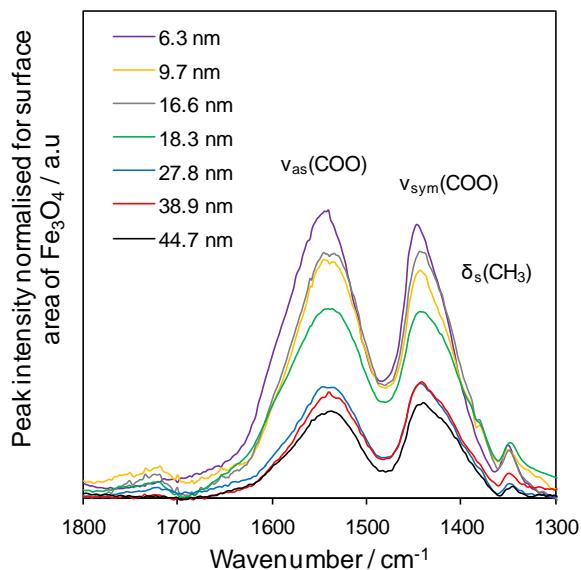


Figure S7. DRIFT spectra of room temperature adsorbed acetic acid over $\text{Fe}_3\text{O}_4/\text{SiO}_2$ catalysts normalised to the Fe_3O_4 surface area (geometric surface areas were estimated from the Fe_3O_4 particle diameter determined by HRTEM, assuming a spherical morphology). Spectra recorded at 200 °C in vacuo to remove physisorbed acid contributions.

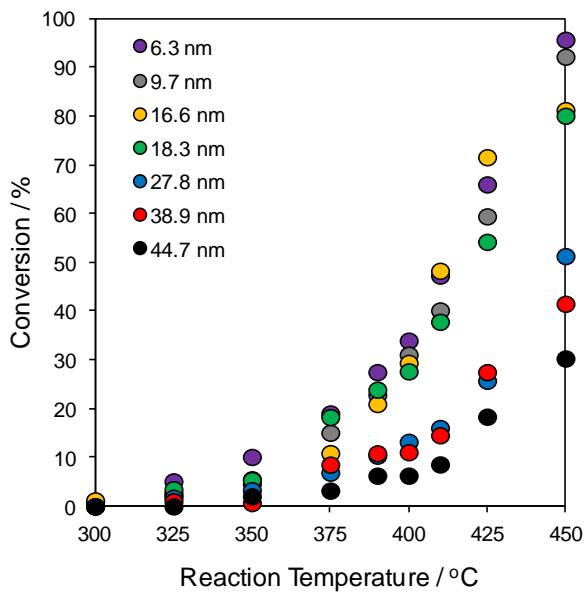


Figure S8. Acetic acid conversion over Fe₃O₄/SiO₂ catalysts of varying Fe₃O₄ particle size at increasing reaction temperatures. Values reported are the average after 1 h reaction at each temperature.

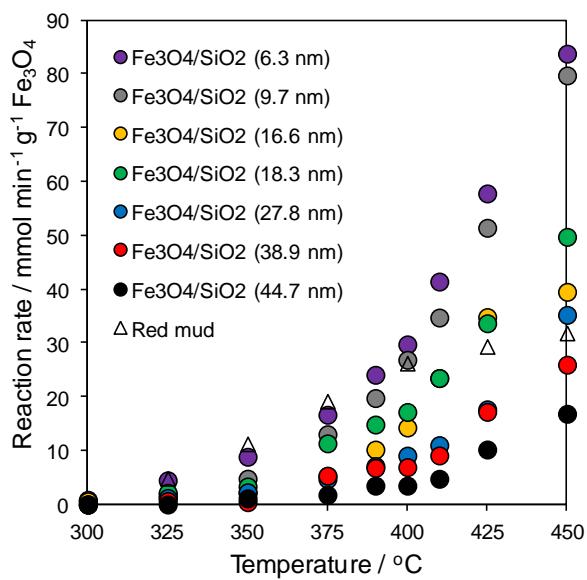


Figure S9. Rate of acetic acid conversion over Fe₃O₄/SiO₂ and Red Mud. Data is normalised for the mass of Fe₃O₄ present in the catalyst. Values reported are the average after 1 h reaction at each temperature.

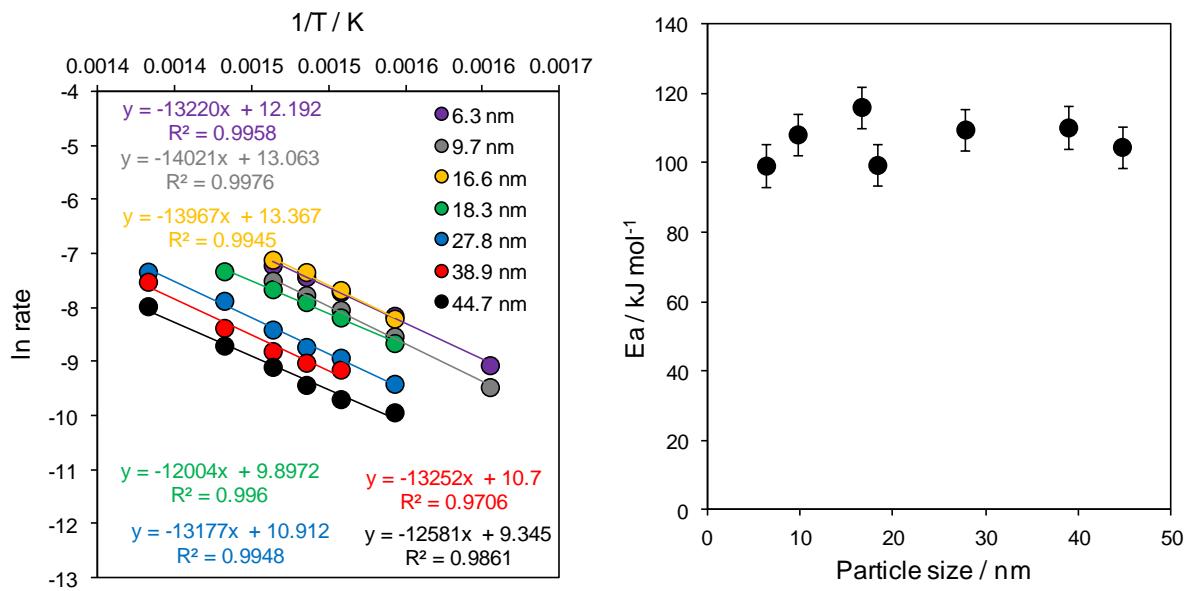


Figure S10. Arrhenius plots (left) and activation energies (right) for acetic acid ketonisation over Fe_3O_4 of increasing particle size. Values are calculated using data corresponding to conversions of 10-50 %.

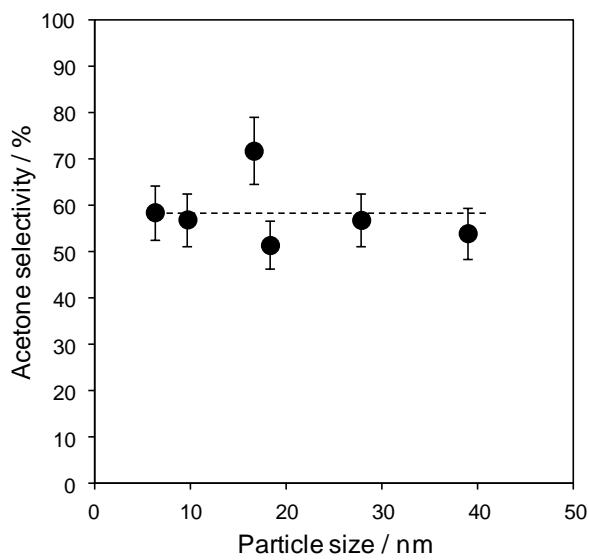


Figure S11. Acetone selectivity vs Fe_3O_4 particle size at an acetic acid conversion of ~50 %.

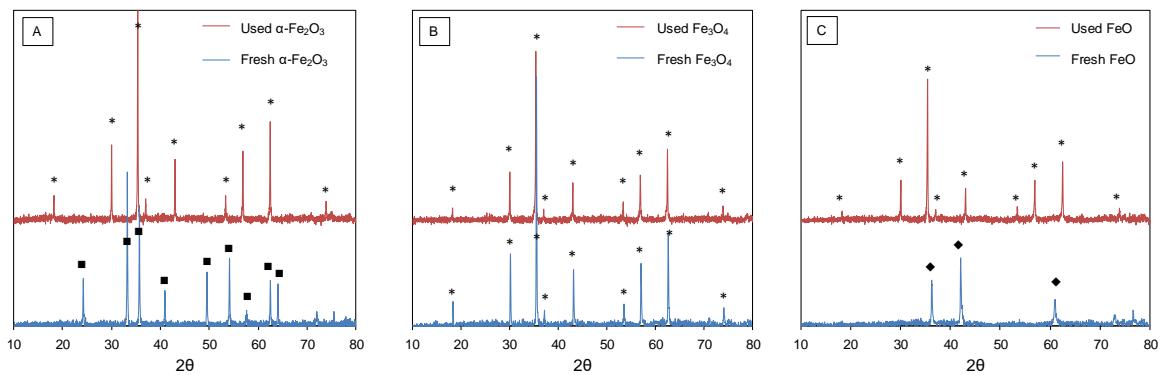


Figure S12. XRD patterns of fresh and used Fe_2O_3 , Fe_3O_4 and FeO ketonisation catalysts. Diffraction peaks corresponding to α - Fe_2O_3 , Fe_3O_4 and FeO phases are indicated with squares (■) asterisks (*) and diamonds (◆) respectively. All used catalysts showed only peaks corresponding to Fe_3O_4 .

Table S1. Estimated Fe_3O_4 surface area for $\text{Fe}_3\text{O}_4/\text{SiO}_2$ catalysts.^a

Fe ₃ O ₄ loading / wt%	4	8	14	28	36	56	63
Fe ₃ O ₄ surface area / $\text{m}^2 \cdot \text{g}_{\text{catalyst}}^{-1}$	7.4	9.7	10.1	17.7	15.1	16.7	16.4
Acid site density / mmols. $\text{g}_{\text{catalyst}}^{-1}$	0.169	0.199	0.256	0.288	0.22	0.251	0.252

^aAssuming spherical particles with diameters from XRD as reported in Table 1 of the main text.

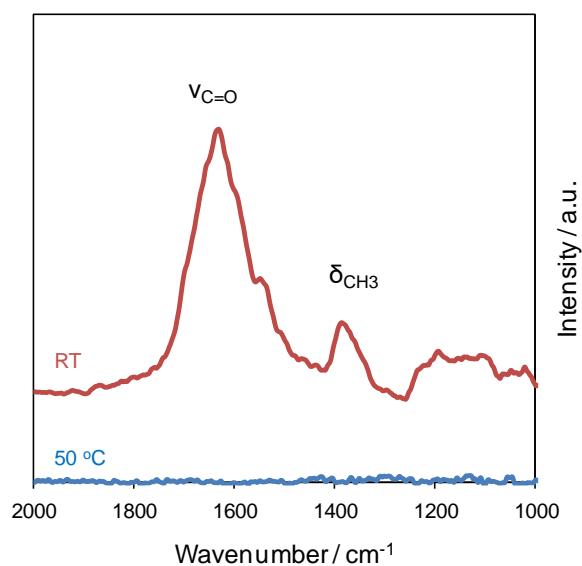


Figure S13. DRIFT spectra of chemisorbed acetone over pure magnetite at room temperature and 50 °C. Bands for molecular acetone are visible at 1631 and 1387 cm^{-1} .