

Response of heat release to equivalence ratio variations in high Karlovitz premixed H₂/air flames at 20 atm

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Nomenclature

β_i	Temperature exponent of Arrhenius equation	K_{ci}	Equilibrium constant
δ_L	Laminar flame thickness	l_t	Integral length scale
δ_f	Reaction layer thickness	$[M]$	Overall contribution of different species in Three-body reactions
Δx	Grid resolution	Re	Reynolds number
κ	Mean curvature	S_L	Laminar flame speed
ν	Kinematic viscosity	S_{yz}	Cross-section area
ν'_{kj}	Forward stoichiometric coefficient for species k in reaction j	T	Local temperature
ν''_{kj}	Reverse stoichiometric coefficient for species k in reaction j	T_u	Temperature of unburnt gas
φ	Equivalence ratio of the fresh mixture	T_b	Temperature of burnt gas
φ_L	Local equivalence ratio	u'	Root-mean-square turbulent velocity fluctuation
$\dot{\omega}$	Species reaction rate	V_{rec}	Reaction zone volume
A_i	Pre-exponential factor of Arrhenius equation	X_k	Molar concentration of species k
c	Progress variable	$Y_{f,k}$	Local mass fraction of species k
E_i	Activation energy of a reaction	$Y_{u,k}$	Mass fraction of species k in the fresh mixture
Ka	Karlovitz number	$Y_{b,k}$	Mass fraction of species k in the burnt mixture
K_f	Forward reaction rate constant		
K_r	Reverse reaction rate constant		
K_0	Limit of low-pressure reaction rate constant		
K_∞	Limit of high-pressure reaction rate constant		

1 **Abstract**

2 This paper presents three-dimensional direct numerical simulations of lean premixed H₂/air
3 flames with equivalence ratio 0.4, 0.5 and 0.6, respectively. The initial Karlovitz number is around
4 2335 and the pressure is 20 atm, which is relevant to gas turbine conditions. The heat release in
5 reaction zones under different equivalence ratios is examined statistically with the aim to extending
6 our understanding of lean combustion under high-pressure conditions. With increasing equivalence
7 ratio, the relative thickness of reaction zone (δ_f/δ_L) is increasing for both laminar and turbulent flames,
8 but the extent of increase is reduced under high equivalence ratio. By examining the local structures
9 of flame fronts, it is found that trenches and plateaus of local equivalence ratio are located on separate
10 sides of the reaction zone edge. Due to the decreased Lewis number under high equivalence ratio, the
11 trench ‘depth’ and plateau ‘height’ are reduced. For the flame under ultra-lean conditions, there are
12 some spots with temperatures above adiabatic temperature. This is attributed to the high-fraction of
13 radicals in these regions, which will promote heat release. Furthermore, the heat release rates of
14 elementary reactions are investigated with the analysis of radical fractions and rate constants. When
15 the mixture equivalence ratio varies, the local heat release is changed in different temperature
16 windows due to the combined effects of radical fractions and reaction rate constants.

17 *Keywords:* Direct numerical simulation; Lean premixed flame; Heat release rate; Equivalence ratio

18

1 **1. Introduction**

2 With growing concern about global climate change and increasingly stringent regulations on
3 pollutant emissions, lean premixed combustion has had wide-ranging applications in industrial
4 devices, e.g. stationary gas turbines [1]. In lean premixed combustion, the peak combustion
5 temperature is reduced, leading to lower NO_x emission. However, turbulent lean premixed flames are
6 susceptible to equivalence ratio oscillation, which is one of the most significant mechanisms
7 contributing to combustion instabilities, and local extinction can occur due to variations of
8 equivalence ratio in combustion chambers [2-4]. In modern gas turbines, typical equivalence ratios
9 at base load are in the range of 0.45-0.6 [2]. The turbulent flames in gas turbines are also characterised
10 by intense turbulence intensity and high pressure [5, 6]. The turbulent velocity fluctuation is as high
11 as 150 times of the laminar flame speed and the pressure can reach up to 30 bar in gas turbines [5-7].
12 Under these critical conditions, flame structures and chemical activities will be dramatically modified
13 [8], and the enhanced turbulence-flame interaction dramatically increases difficulties in experimental
14 and numerical studies. Therefore, it is vital to have a good understanding of fundamental
15 characteristics of lean premixed combustion under conditions relevant to industrial combustion
16 devices, which will promote combustion device developments and combustion model validations.

17 One crucial unsolved issue in combustion instability is the heat release rate variation with the
18 equivalence ratio, despite numerous experimental and numerical studies [9]. In such a context, a non-
19 dimensional parameter, the Karlovitz number (Ka) [10], was introduced to describe the time scales
20 of flame-turbulence interactions. Under conditions relevant to gas turbines, the Karlovitz number
21 tends to increase to a high level, and turbulent flames will move from the thin reaction zone ($1 < Ka$
22 < 100) towards the distributed reaction zone ($Ka > 100$). It is demonstrated by Stopper et al. [11] that
23 the Karlovitz number is in the range of 77-230 in a swirl burner for industrial gas turbines. Zhou et
24 al. [12] experimentally studied high Ka jet flames with equivalence ratio (ϕ) 0.4 and 0.7. They found
25 that, under high Ka, rapid transport can significantly change the distribution of radicals and heat
26 release is enhanced in low-temperature regions. Under leaner conditions, it is easier for the flames to

1 become distributed. Skiba et al. [13] measured the Bunsen-type flame structures in 16 cases with φ
2 = 0.65 and 0.85. They found that the preheat zone is dramatically broadened at high Ka, especially at
3 higher equivalence ratio. However, the thickness of the reaction layer is insensitive to turbulence
4 intensity even though the layer was seriously distorted at high Ka. Zheng et al. [14] studied premixed
5 H₂/air flames under various equivalence ratios in an explosion duct. Under certain ignition positions,
6 typical tulip flames could be formed under fuel lean and fuel ultra-rich conditions, while no tulip
7 flames could be formed under slightly rich conditions. Song et al. [15] investigated flame propagation
8 characteristics of hydrogen enriched natural gas with $\varphi = 0.8 - 1.2$. Maximum flame speed was
9 observed under stoichiometric condition and the speed decreases in leaner and richer flames. Under
10 lean conditions, the flame becomes unstable due to the decreased Markstein length.

11 Due to the difficulty of performing fundamental studies under both high turbulent intensities and
12 high pressures, most of high-Ka experiments are performed at atmospheric pressure or slightly
13 elevated pressures [16-18]. The experimental system for high Ka and high pressure is usually
14 expensive and complicated. Recently, the development of supercomputing enables three-dimensional
15 (3D) direct numerical simulation (DNS) of turbulent flames with detailed chemistry, which helps to
16 obtain detailed flame information that is expensive and difficult to get through experiments. DNS
17 solves the full Navier-stokes equations, resolves turbulence from the integral length scale to
18 Kolmogorov length scale, and could also reveal the local heat release from different chemical
19 pathways. Wang and Luo et al. [19, 20] applied DNS to investigate hydrogen/air premixed flames
20 with equivalence ratio 0.6 and 1.0 at moderate Ka. Due to the effects of differential diffusion, flames
21 under lean conditions burn more vigorously in convex regions toward the unburned gas compared
22 with the stoichiometric flames. The flame becomes diffusive-thermally unstable when combustion
23 happens under lean conditions. Aspden et al. [21-23] conducted a series of DNS cases at moderate
24 and high Ka under ultra-lean conditions $\varphi = 0.31$ and 0.4. It is found that the area of intense reaction
25 in flow direction is decreased when the initial equivalence ratio increases from 0.31 to 0.4. With

1 increasing turbulence intensity, the density gradient across the reaction zone at $\varphi = 0.4$ decreases,
2 which is opposite to the trend at $\varphi = 0.31$.

3 The aforementioned studies have provided valuable information about the heat release
4 characteristics of premixed flames at high Ka under various lean conditions. However, most of the
5 reported experimental and numerical studies in literature are typically at atmospheric pressure which
6 is far below the operation condition of gas turbines. At elevated pressures, the flame thickness and
7 speed are dramatically changed, which will modify the flame-turbulence interaction significantly.
8 Dinesh et al. [24, 25] applied 3D DNS to premixed spherical flames at 4 atm with various equivalence
9 ratios. They found that the flame front curvature shows a positive correlation with heat release rate
10 under lean conditions. However, this study is performed in the thin reaction zone with moderate Ka.
11 Wang et al. [4, 26, 27] extended DNS to turbulent combustion at 20 bar with equivalence ratios in
12 the range of 0.39-0.5. Some cases were performed with high turbulence intensity which is relevant to
13 lean-burn natural gas engines. However, these researches focus on flame speed and flame front
14 structures instead of heat release characteristics. The response of heat release to equivalence ratios in
15 high-Ka flames under high pressures is yet to be clarified.

16 In the present study, DNS of lean premixed H₂/air flames with detailed chemistry is performed
17 under conditions relevant to stationary gas turbines [2]. The focus of this paper will be on the
18 characteristics of heat release and reaction zones with various equivalence ratios. The initial Ka
19 number is around 2335 and the pressure is 20 atm. The paper is organized as follows. Numerical
20 methods and computational parameters are introduced in Section 2. In Section 3, the local and overall
21 heat release characteristics of flames under different equivalence ratios are discussed. Moreover, the
22 kinetic parameters and radical fractions of major elementary reactions are presented. In the final
23 section, conclusions of this work are given.

24 **2. Numerical approach**

25 *2.1. Direct numerical simulation*

1 The simulations presented in this work are carried out using the DNS code PENCIL [28]. The
 2 compressible Navier-Stokes equations coupled with detailed transport properties and chemical
 3 kinetics are solved using a six-order explicit finite difference scheme. To reduce computational cost,
 4 mixture-averaged species transport model is adopted for species diffusion in this study, ignoring Soret
 5 and buoyancy effects. Aspden et al. [21, 22] illustrated that the mixture-averaged transport model
 6 could retain much of the qualitative behavior of lean H₂/air flames at high Ka. Preliminary analysis
 7 of laminar flames (not shown here for the sake of brevity) also indicates that the effects of equivalence
 8 ratio are qualitatively obtained even if the Soret diffusion is neglected. Moreover, it is demonstrated
 9 that the influence of buoyancy is significantly reduced in flames with high turbulence intensity,
 10 especially for flames in small scales [29-31]. Low-storage third-order Runge-Kutta (RK3-2N) scheme
 11 is used for time advancement and Livermore Solver for Ordinary Differential Equations (LSODE) is
 12 adopted for chemistry calculation.

13 The adopted chemical mechanism of H₂/O₂ was developed by Li et al. [32], which is widely used
 14 in the study of H₂ oxidation under various conditions [33-36]. Ströhle and Myhrvold [37] evaluated
 15 several detailed H₂/O₂ reaction mechanisms under gas turbine conditions, and they found that Li's
 16 mechanism shows the best agreement with experimental data in the investigation of both ignition
 17 laminar flame speed and delay time. This mechanism contains 21 reversible reactions and 9 species.
 18 In the present study, the species reaction rate is given by [38, 39]:

$$19 \quad \dot{\omega} = \sum_{j=1}^M \left(K_f \prod_{k=1}^N [X_k]^{v'_{kj}} - K_r \prod_{k=1}^N [X_k]^{v''_{kj}} \right) \quad (1)$$

20 where K_f and K_r are forward and reverse reaction rate constants for reaction j . v'_{kj} and v''_{kj} are forward
 21 and reverse stoichiometric coefficients for species k in reaction j . X_k is the molar concentration of
 22 species k . Basically, the K_f is expressed as:

$$23 \quad K_f = A_i T^{\beta_i} \exp(-E_i/R_c T) \quad (2)$$

24 where A_i , β_i , E_i , R_c and T are the pre-exponential factor, temperature exponent, activation energy,
 25 gas constant and temperature respectively.

1 In some dissociation or recombination reactions, a ‘third body’ is usually required. In this case,
 2 a new factor $[M]$ is introduced to Equation 1 to determine the reaction rate:

$$3 \quad \dot{\omega} = \sum_{j=1}^M [M] \left(K_f \prod_{k=1}^N [X_k]^{v_{kj}} - K_r \prod_{k=1}^N [X_k]^{v_{kj}} \right) \quad (3)$$

4 where $[M]$ represents the overall contribution of different species as third bodies. In this study, the
 5 values of $[M] \cdot K_f$ and $[M] \cdot K_r$ are regarded as forward and reverse reaction rate constants for three-
 6 body reactions.

7 For the pressure-dependent reactions in the used mechanism, the forward rate constant is
 8 determined by:

$$9 \quad K_{fh} = \left(\frac{K_0[M]}{K_\infty + K_0[M]} \right) F \quad (4)$$

10 where K_0 and K_∞ are the limits of low-pressure and high-pressure rate constants, which are calculated
 11 by Equation 2. In this study, the TROE approach [40, 41] is adopted to determine the factor F , which
 12 is more realistic and compact enough in analysing large reaction systems.

13 For the reversible reactions, the rate constant is given by:

$$14 \quad K_r = K_f / K_{ci} \quad (5)$$

15 where K_{ci} is the equilibrium constant which is determined from thermodynamic properties in this
 16 study.

17 The chemistry implementation was validated quantitatively with Chemkin [39]. The sample
 18 applications of PENCIL code in premixed turbulent combustion could be found in [7, 28, 31, 42, 43].

19 2.2. Simulation parameters

20 Three simulations are performed in configurations with an aspect ratio of 2:1:1 as shown in Fig.
 21 1. In order to initialise the domain, isotropic turbulence with fluctuation u' is pre-generated using
 22 helical forcing functions[44]. In addition, laminar flames are also desired to initialise the chemistry
 23 of turbulent flames. Periodic boundary conditions are applied in lateral directions, and non-reflecting
 24 Navier-Stokes Characteristics Boundary Conditions (NSCBC) [45] are applied at the inlet/outlet to

1 maintain the high pressure. The domain width is set to be 10 times of the integral length scale, which
 2 is higher than that of reported simulations with similar configurations [4, 42, 43, 46]. The parameters
 3 of DNS database are listed in Table 1. For all the three cases, the initial pressure is 20 atm, which is
 4 relevant to stationary gas turbines. The temperature of unburnt gas is $T_u = 298$ K and the equivalence
 5 ratio varies from 0.4, 0.5 to 0.6. The turbulent Reynolds number (Re) and Karlovitz number (Ka) [47]
 6 are defined as:

$$7 \quad \text{Re} = u' l_t / \nu \quad (6)$$

$$8 \quad \text{Ka} = (u'^3 / \nu l_t)^{1/2} / (S_L / \delta_L) \quad (7)$$

9 where u' is the root-mean-square turbulent velocity fluctuation, l_t the integral length scale, ν the
 10 kinematic viscosity, S_L the laminar flame speed and δ_L the laminar flame thickness. The flame
 11 thickness is defined by $\delta_L = (T_b - T_u) / |\nabla T|_{\max}$, where T_b and T are the burnt gas temperature and local
 12 temperature, respectively.

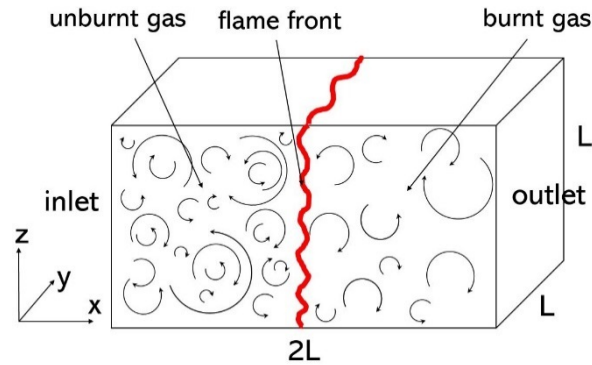


Fig. 1 - Schematic of the simulation domain.

13 In order to study the effects of equivalence ratio independently, the Karlovitz number and l_t/δ_L
 14 are fixed for the three simulations at different equivalence ratios. However, the Reynolds number is
 15 higher when the equivalence ratio is increased. To save computational resources, the ratio l_t/δ_L , is
 16 kept unity, which is also used in other DNS studies [48-50]. Figure 2 shows that the three cases are
 17 located in the distributed reaction zone with high u'/S_L ratio, which is more relevant to combustion
 18 in real combustors. With the increasing equivalence ratio, the laminar flame speed is increasing while
 19 the laminar flame thickness is decreasing. Correspondingly, the turbulent velocity fluctuation
 20 increases dramatically.

Table 1- Simulation parameters.

Case	A	B	C
Equivalence ratio (ϕ)	0.4	0.5	0.6
Laminar flame speed (S_L) (cm/s)	1.66	6.81	21.16
Laminar flame thickness (δ_L) (cm)	2.54E-02	8.3E-03	3.3E-03
Root-mean-square turbulent velocity fluctuation (u') (cm/s)	177	664	1941
Kinematic viscosity (ν) (cm ² /s)	9.05E-03	9.34E-03	9.62E-03
Integral length scale (l_t) (cm)	2.54E-02	8.3E-03	3.3E-03
Grid resolution (Δx) (μm)	4.96	3.24	1.29
Turbulent Reynolds number (Re)	497	590	666
Karlovitz number (Ka)	2376	2373	2368

1 The domain length is 20 times the corresponding integral length scale. The domain is then
2 discretised by uniform grids of $1024 \times 512 \times 512$ for case A and $512 \times 256 \times 256$ for cases B and C.
3 As a result, the grid resolution decreases from 4.96 to 1.29 μm . To resolve the chemical scales, there
4 are over 26 grid points across the flame thickness, which was also used for the high Ka flames in Ref.
5 [21]. The time step is controlled by the Courant-Friedrichs-Lewy condition for computational stability.
6 As in our previous work [7, 31], before we run the three-dimensional simulations, grid-independent
7 tests were also carried out in two-dimensional domains to make sure the mesh used here can produce
8 grid-independent results. The analysis is done at the time corresponding to 2 eddy turn-over time $t =$
9 $2\tau_l$ ($\tau_l = l_t / u'$) for the three cases. Carlsson et al. [46, 51] studied H₂/air flames under high Ka. They
10 found that the flames develop rapidly in the turbulence, and a fully evolved turbulent flame could be
11 obtained within $0.2 < t / \tau_l < 0.4$. It was demonstrated by Rutland et al. [52] that the time is slightly
12 longer than one eddy turnover time for numerical simulation of turbulent premixed flames to achieve
13 equilibrium status. As in our previous work [7], it was found that the mean and statistical values show
14 monotonic variation with time after $t / \tau_l = 2$. The key information of flame front structures and
15 chemical pathways could be qualitatively captured at $t = 2\tau_l$.

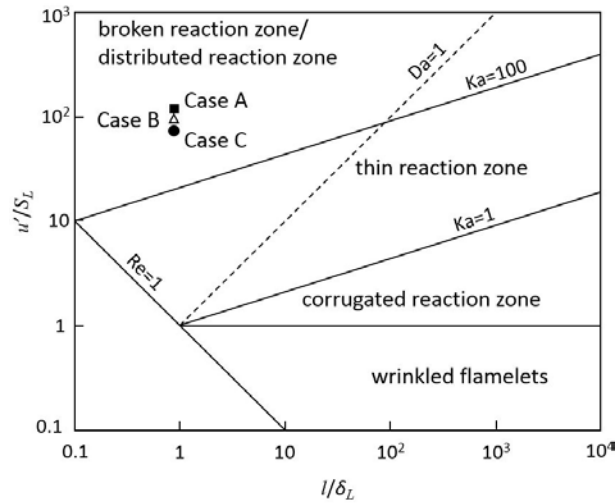


Fig. 2 - Turbulent combustion regime diagram with locations of current simulation cases.

3. Results and discussion

3.1. Overview of laminar and turbulent flames

As the turbulent flames are initialized with laminar flames, we firstly discuss the flame characteristics of laminar flames before we explore the turbulent flames. Figure 3 shows the temperature and heat release rate (HRR) profiles of laminar flames at equivalence ratio 0.4, 0.5 and 0.6, where the abscissa values are scaled by the corresponding laminar flame thickness. Table 2 lists the key parameters of the reaction zones. As expected, the burnt gas temperature increases from 1530 K to 1836 K and the HRR is dramatically enhanced when the equivalence ratio increases from 0.4 to 0.6. Correspondingly, the scaled temperature gradient in Fig. 3 is larger under higher equivalence ratio to ensure the same scaled thermal thickness δ_L . However, it should be noted that the reaction zone is thinner than thermal thickness in the studied cases. Hereby, the reaction zone is defined as regions with heat release rate higher than 10% threshold of corresponding laminar flames. When the equivalence ratio increases, the reaction zone is obviously broadened. As shown in Table 2, the reaction layer thickness of laminar flames increases from $0.54 \delta_L$ to δ_L when the equivalence ratio increases from 0.4 to 0.6. Moreover, two characteristic temperatures of laminar flames are presented. The temperature corresponding to maximum temperature gradient fluctuates around 1200 K; the temperature corresponding to peak heat release rate increases with increasing equivalence ratio, from 1403 K to 1543 K.

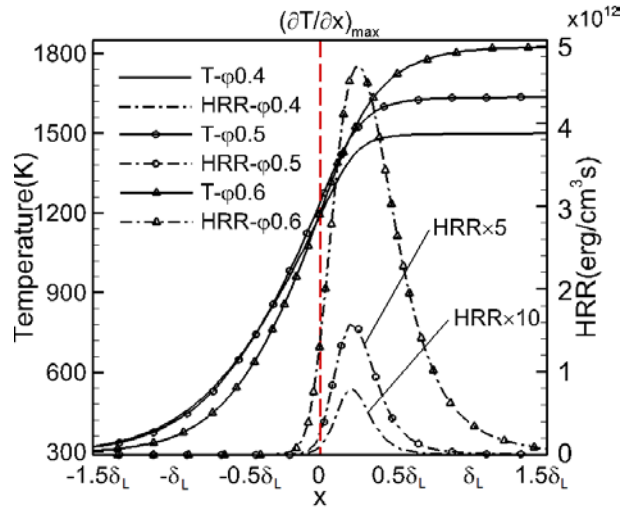


Fig. 3 - Structures of lean premixed laminar flames at different equivalence ratios. The red dashed line denotes the abscissa value which corresponds to the maximum temperature gradient.

1 Next, the reaction zone characteristics of turbulent flames with $\phi = 0.4, 0.5$ and 0.6 are discussed.

2 Figure 4 presents the reaction layer structures coloured by temperature and Fig. 5 shows the mean
3 heat release rate versus progress variable which is defined as:

$$4 \quad c = (Y_{u,H_2} - Y_{f,H_2}) / (Y_{u,H_2} - Y_{b,H_2}) \quad (8)$$

5 where Y_{u,H_2} is the H_2 mass fraction in the fresh mixture, Y_{f,H_2} is the local H_2 mass fraction and Y_{b,H_2}
6 is the H_2 mass fraction in the burnt gas.

Table 2 - Characteristic parameters of reaction zones of laminar and turbulent flames

Case	HRR _{max_1D} (erg/cm ³ s)	Mean HRR _{max_3D} (erg/cm ³ s)	δ_{f_1D}	δ_{f_3D}	T_1 (K)	T_2 (K)
A	7.90E10	3.69E11	0.54 δ_L	1.25 δ_L	1188	1403
B	7.87E11	1.95E12	0.65 δ_L	1.63 δ_L	1238	1478
C	4.68E12	6.73E12	δ_L	1.86 δ_L	1196	1543

δ_f - reaction layer thickness

Mean HRR_{max_3D} - maximum conditional mean of HRR on progress variable in turbulent flames

T_1 - temperature corresponds to maximum temperature gradient of laminar flames

T_2 - temperature corresponds to peak heat release rate of laminar flames

1 Table 2 also gives the key parameters of turbulent flames. The average reaction layer thickness
2 of turbulent flame is defined as $\delta_f = V_{rec} / S_{yz}$, where the reaction zone volume V_{rec} is the volume of
3 regions with heat release higher than 10% threshold of the corresponding laminar flames and the
4 cross-section area $S_{yz} = L^2$ is the area of y-z slice across the domain as shown in Fig. 1. For laminar
5 flames, the reaction layer thickness is determined directly from the profile of heat release rate versus
6 flame position x . Since the three cases are characterized by the same Ka, the flame fronts show
7 analogous structures in Fig. 4. Similar to the laminar flames, the heat release of turbulent flames is
8 enhanced, and the reaction layer is relatively broadened under high equivalence ratio.
9 Correspondingly, the reaction zone covers a wider range of temperature at high ϕ . These differences
10 under various equivalence ratios are attributed to the differential diffusion effect in premixed
11 combustion [20]. In Fig. 5, obvious heat release is observed from $c = 0.4$ for case $\phi = 0.6$ while it
12 happens after $c = 0.7$ for case $\phi = 0.4$. It is also noted that the reaction layers of turbulent flames are
13 thicker than the corresponding thermal thicknesses, and the thickness increases with increasing
14 equivalence ratio. Although the turbulent flames exhibit similar trends to laminar flames with varying
15 equivalence ratios, the extent of enhancement is reduced at high equivalence ratio. For example, the
16 peak conditional mean of heat release rate for the turbulent flame with $\phi = 0.4$ is 3.7 times higher
17 than that of the corresponding laminar flame, while the value is only 0.4 times higher for the turbulent
18 flame with $\phi = 0.6$. The reaction layer thickness almost doubles in the laminar flames when the
19 equivalence ratio increases from 0.4 to 0.6. For the turbulent flames, the thickness only increases
20 from $1.25 \delta_L$ to $1.86 \delta_L$. One possible explanation is that the enhanced heat release of turbulent H₂/air
21 flame is a combined result of turbulent transport and species diffusion, but the turbulent transport is
22 overtaking differential diffusion as the main effect when the flame transitions to the distributed
23 reaction mode.

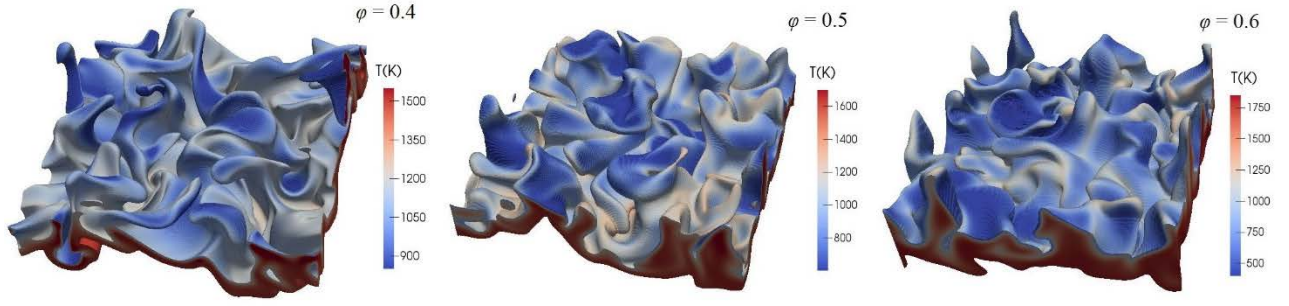


Fig. 4 - Reaction zone structures of lean premixed turbulent flames at different equivalence ratios.

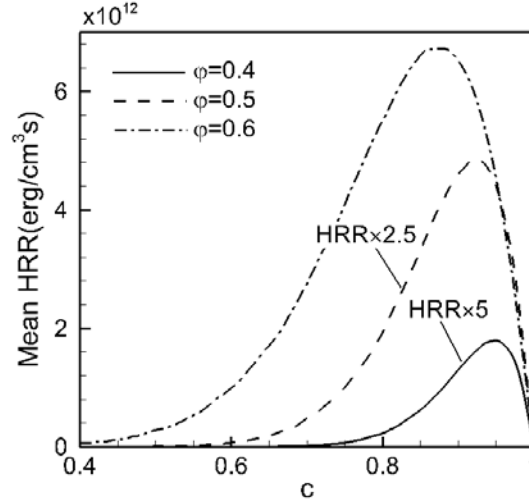


Fig. 5 - Conditional mean of heat release rate on progress variable for turbulent flames at different equivalence ratios.

3.2. Characteristics of turbulent reaction zones

In this section, we discuss the local and statistical values regarding the heat release in turbulent reaction zones. Figure 6 shows the zoomed-in contours of local equivalence ratio in the flame brush, where the reaction layers are bounded by the white solid lines and the local ϕ plateaus ($\phi_L > 1.1 \phi$) are bounded by the solid black lines. The local equivalence ratio ϕ_L is defined as:

$$\phi_L = \frac{Y_H / (2 \cdot W_H)}{Y_O / W_O} \quad (9)$$

where Y_H and Y_O are mass fractions of hydrogen and oxygen element, and W_H and W_O are molar mass of hydrogen and oxygen element, respectively. The contours indicate the presence of differential diffusion in the studied cases. It is obviously noted that ϕ_L is significantly lower than the fresh gas ϕ in the upstream near the reaction layer and all the ϕ_L plateaus of the three cases locate in the reaction

1 layer. Hereby, we define the left boundary of the reaction zone as ' φ_L cliff', the convex region towards
 2 the unburned side is characterised by positive curvature and the concave region is characterised by
 3 negative curvature. It is interesting to find that the φ_L trenches and plateaus are situated on both sides
 4 of the cliff, which is much like the natural topography. The temperature gradient near φ_L cliff is
 5 observed to be high at positive curvatures, and low at negative curvatures. However, the difference
 6 in temperature gradient between positive and negative curvatures is reduced with increasing φ .
 7 Furthermore, the trench 'depth' and plateau 'height' are reduced as the φ is increased. This is
 8 primarily due to the decrease of the Lewis number with increasing φ , which promotes a diffusive-
 9 thermally stable flame [19].

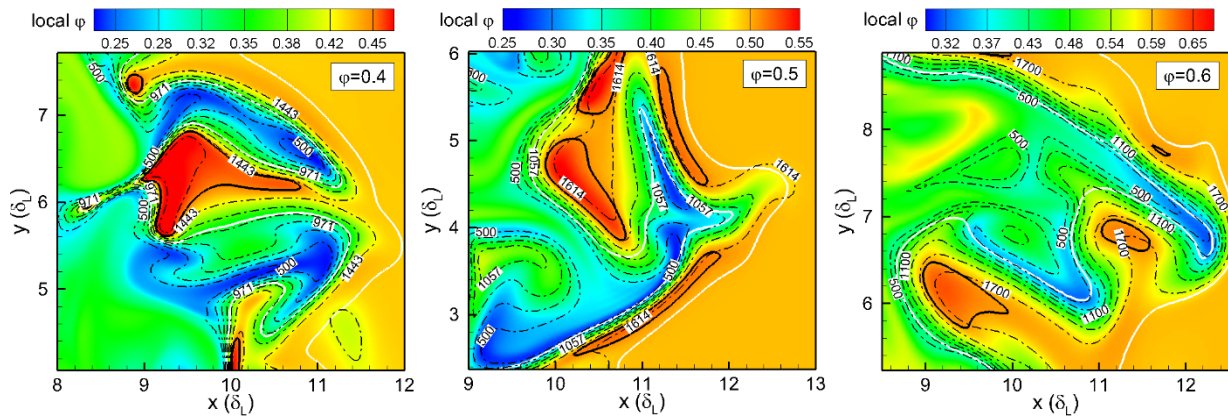


Fig. 6 - Two-dimensional slices of the reaction zone coloured by local equivalence ratio. The black dashed lines correspond to temperature levels, the solid black lines bound the local φ plateaus and the white solid lines bound the reaction zone.

10 Since the φ_L cliff area is also characterized by a high gradient of temperature in Fig. 6, it is
 11 necessary to shed more light on the correlation of temperature, φ_L and heat release rate. Figure 7
 12 shows the scattered φ_L versus temperature in the reaction zone, where the scatters are coloured by
 13 local heat release rate. The adiabatic temperature of the corresponding laminar flame is also indicated
 14 in the plots. Overall, the scatter distribution shows a positive correlation between φ_L and temperature
 15 for the three cases. Nevertheless, the broader scatter distribution of Case $\varphi = 0.6$ indicates that the
 16 correlation rate is reduced when φ is increased. It is interesting to note that there are many hot spots
 17 above the adiabatic temperature under leaner conditions. For example, for Case $\varphi = 0.4$, the adiabatic

1 laminar flame temperature is 1530 K, while the peak temperature of the turbulent flame exceeds 1800
 2 K. On the other hand, the temperature of the whole reaction zone is below the adiabatic temperature
 3 for Case $\varphi = 0.6$. A similar trend was also reported by Aspden et al. [21] for lean premixed H_2 /air
 4 flames under atmospheric pressure. In their study, hot spots appear under ultra-lean condition ($\varphi =$
 5 0.31) despite Ka. At $\varphi = 0.4$, hot spots are observed at low to moderate Ka, while they disappear in
 6 distributed flames. In the current study, hot spots still exist in the high-Ka flames at $\varphi = 0.4$ and 0.5,
 7 which is mainly attributed to the pressure effects on reaction zone structures. As mentioned before,
 8 lean-premixed combustion has the potential to reduce NO_x emission due to low peak combustion
 9 temperature. However, temperature in the hot regions under ultra-lean conditions (Case $\varphi = 0.4$)
 10 would exceed the adiabatic temperature to a large extent, which will contribute to the formation of
 11 NO_x . This result is instructive and meaningful for industrial application of lean-premixed combustion.

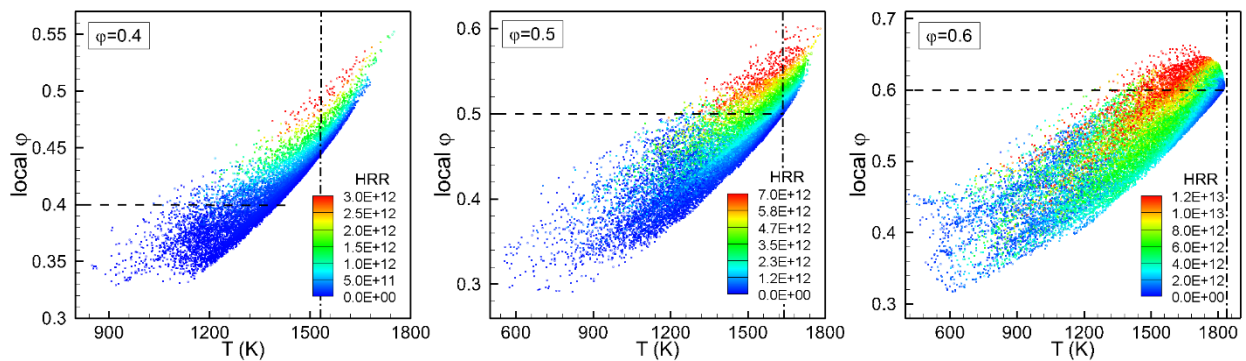


Fig. 7 - Scatter plots of local temperature and local equivalence ratio in the reaction zone. The scatters are coloured by local heat release rate. The horizontal dashed lines denote the equivalence ratio in the unburned gas and the vertical dashed lines denote the peak temperatures of the corresponding laminar flames.

12 The presence of hot spots is a consequence of extended φ_L above unburnt mixture φ under leaner
 13 condition. As indicated in Fig. 7, the φ_L extends to about 0.15 higher than the mixture φ for Case $\varphi =$
 14 0.4, while the value is only around 0.05 for Case $\varphi = 0.6$. As the Lewis number is decreasing with
 15 increasing equivalence ratio, the diffusion of light species (e.g. H_2 , H) will be enhanced at $\varphi = 0.6$
 16 and the reaction zone will be broadened as seen on Table 2. As a result, the species distribution and
 17 heat release are more uniform in the reaction zone. By contrast, the heat release is more intense in

1 the narrow reaction zone and hot spots appear at $\varphi = 0.4$. Furthermore, the heat release rate shows a
 2 positive correlation with both temperature and φ_L . However, the HRR gradient is decreasing across
 3 temperature with increasing φ . For example, the tail of Case $\varphi = 0.6$ in Fig. 7 is coloured by blue and
 4 green (low and moderate HRR), while the tail of Case $\varphi = 0.4$ is only coloured by blue (low HRR).
 5 This observation agrees with the results shown in Fig. 6. For high-Ka flames at atmospheric pressure,
 6 turbulence transport is becoming dominant and the effects of differential diffusion is diminishing [51,
 7 53]. However, the profiles of local equivalence ratio in Fig. 7 illustrate that differential diffusion is
 8 still significant in the current high-Ka cases at 20 atm, which is attributed to the thinner reaction
 9 regions at high pressures.

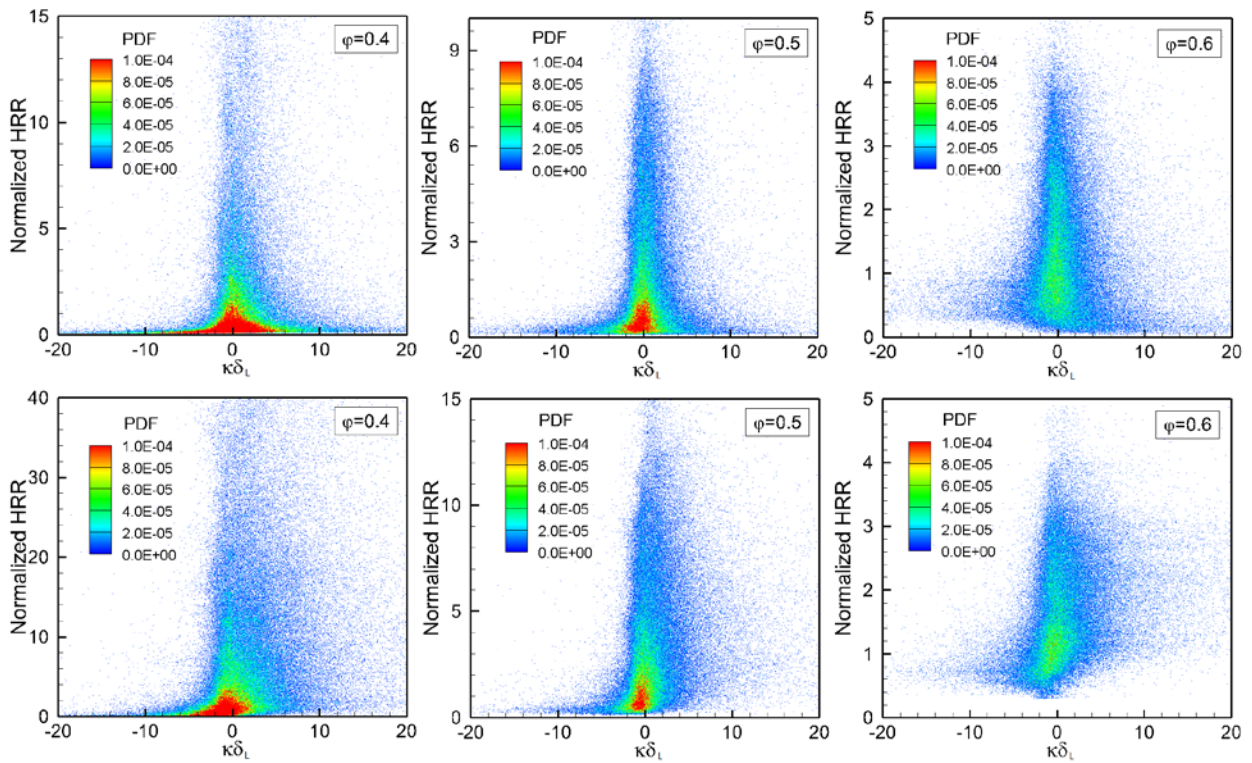


Fig. 8 - Scatter plots of curvature and normalised heat release rate on the iso-surfaces with corresponding temperature T_1 (top row) and T_2 (bottom row) as indicated in Table 2. The curvature is scaled by the corresponding laminar flame thickness.

10 To shed more light on the effects of flame structures on the heat release rate, two temperature
 11 iso-surfaces in the reaction zone are selected, and the probability density function (PDF) for scaled
 12 curvature and normalised HRR is shown in Fig. 8. The two temperatures, T_1 and T_2 as indicated in

1 Table 2, respectively, correspond to maximum temperature gradient and peak heat release rate in
2 laminar flames. The mean curvature is defined as $\kappa = -\nabla \cdot \hat{n}$, where $\hat{n} = -\nabla T / |\nabla T|$ is the unit normal
3 vector of the flame front. In Fig. 8, the mean curvature is scaled by the corresponding laminar flame
4 thickness and the value is positive for the convex regions towards the unburned side. For iso-surfaces
5 of T_1 , the scatters show a normal distribution for Case $\varphi = 0.4$ and 0.5 , although the HRR of positive
6 curvatures is relatively higher than that of negative curvatures. Nevertheless, the behaviour of the
7 heat release rate distribution for Case $\varphi = 0.6$ differs from the other two cases. The lowest HRR
8 occurring in positive curvature regions is higher than that in negative curvature regions. It should be
9 noted that the PDF gradient is decreasing with increasing equivalence ratio, which means the
10 enhancement (weakening) of reaction rate in convex (concave) regions is reducing as equivalence
11 ratio is increased. This finding is consistent with the results of Luo et al. [20] for H₂/air flames under
12 lean and stoichiometric conditions at the atmospheric pressure. Dinesh et al. [25] also observed weak
13 burning structures in concave regions under lean conditions in spherical flames under elevated
14 pressures.

15 On iso-surfaces of T_2 , the aforementioned trends still exist and become more obvious. The HRR
16 in convex regions is significantly enhanced even for Case $\varphi = 0.6$. Moreover, the peak HRR happens
17 in low curvature regions, which is due to the effects of the Markstein number [48]. Comparing the
18 ordinate values of the two set plots, it is found that the gap is decreasing with increasing equivalence
19 ratio. For example, the ordinate threshold increases from 15 to 40 as the temperature increases from
20 T_1 to T_2 at $\varphi = 0.4$, while the threshold reaches the same value 5 at $\varphi = 0.6$. It indicates that the heat
21 release gradient is specially reduced under high equivalence ratio. Overall, the response of HRR to
22 local curvature is changing with equivalence ratio and either set of the iso-surfaces can present the
23 trend of change.

24 In Fig. 6, the isoline of T_1 is very close to the left boundary of the reaction layer. Thus, flame
25 front structures are statistically identified by the T_1 iso-surface for the three cases. Figure 9 presents
26 the probability density functions (PDFs) of flame front curvatures. The mean curvatures are scaled

1 by the thickness of corresponding laminar flames. The statistical result shows that the flame front
 2 structures are quite similar in the three flames, despite the peak value for flame $\varphi = 0.5$ is a little bit
 3 smaller. Similar distribution is also observed by Wang et al. [4] in lean premixed methane/air flames
 4 with $\varphi = 0.39 - 0.5$ under low Ka. It indicates that the variation of equivalence ratio can not change
 5 flame front wrinkling in both thin reaction zone and distributed reaction zone when Ka is fixed.

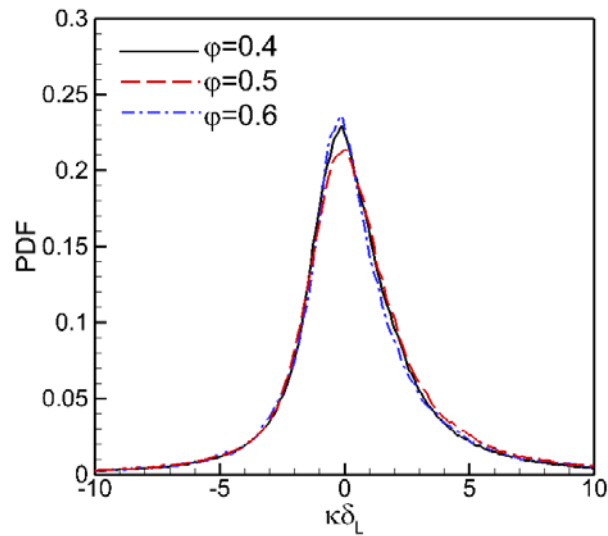


Fig. 9 - PDFs of mean curvatures of flame fronts for cases under different equivalence ratios. The mean curvatures are scaled by corresponding laminar flame thicknesses.

6 3.3. The response of elementary reactions to equivalence ratio variation

7 As a multi-step chemical mechanism is adopted in this study, the heat release we mentioned
 8 above is the overall presentation of all the elementary reactions. When the equivalence ratio varies,
 9 the radical distribution and elementary reaction must be affected. Studying the heat release from main
 10 elementary reactions will extend our understanding of premixed flames. There are 21 reversible
 11 reactions in the used mechanism and the five elementary reactions listed in Table 3 contribute to ~90%
 12 of the total heat releases.

Table 3 Main reactions of Li et al. H₂/O₂ mechanism

#	Reaction	#	Reaction
Reaction3 (R3)	$H_2 + OH = H_2O + H$	Reaction8 (R8)	$H + OH + M = H_2O + M$
Reaction9 (R9)	$H + O_2 (+M) = HO_2 (+M)$	Reaction11 (R11)	$HO_2 + H = OH + OH$

1 Firstly, Figure 10 presents the average heat release rate of the selected 5 elementary reactions
 2 versus temperature in the reaction zones of turbulent flames at different equivalence ratios. As
 3 expected, the elementary reactions show high HRR above the adiabatic temperature in Case $\varphi = 0.4$
 4 and 0.5, which will contribute to the hot spots in the reaction zones. Before reaching the adiabatic
 5 temperature, every reaction exhibits a HRR peak. It is noticed that the HRR peak arises from 1200 K
 6 for all the three cases, while the slope is decreasing with increasing equivalence ratio. Moreover, the
 7 heat release under moderate temperatures (600-1200 K) is significantly enhanced when the
 8 equivalence ratio is increased from 0.4 to 0.6, especially for the dominating reactions R9 and R13. In
 9 the high-temperature regions ($T > 1200$ K), the heat release contributions from R3 and R8 are more
 10 prominent with increasing equivalence ratios. R3 overtakes R13 as the second most dominating
 11 reaction in Case $\varphi = 0.6$.

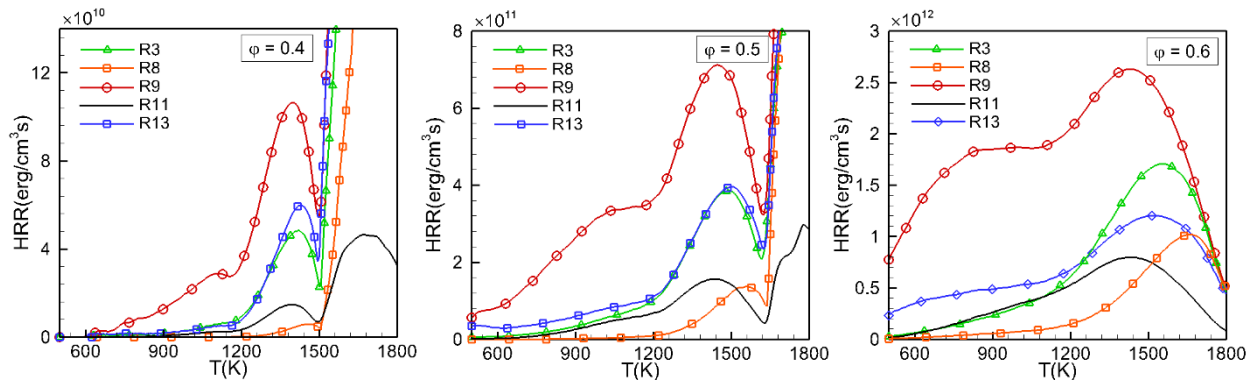


Fig. 10 – Conditional mean of heat release rate on temperature for elementary reactions in turbulent flames.

12 As shown in Eqs. 1 and 3, two key factors, rate constant K and species concentration X_k , directly
 13 determine the reaction rate. Thus, the species concentrations and rate constants as a function of
 14 temperature are presented in Figs. 11 and 12 to assist the discussion of heat release in reaction zones.
 15 Overall, it is seen in Fig. 11 that the fractions of all species are obviously increased with increasing
 16 equivalence ratio, which can explain the enhanced heat release rate under high φ . When the
 17 temperature is higher than adiabatic temperature, it is noted that there exist considerable radicals for
 18 Case $\varphi = 0.4$ and 0.5, which will lead to the formation of hot spots in the reaction zone. This

1 observation is consistent with the φ_L plateaus in Fig. 6. Although differential diffusion is expected to
2 be less important under high Ka [21], the effects are still considerable when the equivalence ratio is
3 increased in this study. From Fig. 11, it is evident that the diffusion of H and OH is enhanced under
4 high φ , leading to a broader and uniform distribution.

5 In Fig. 12, it is seen that the rate constants of reverse reactions are negligible compared with that
6 of forward reactions, despite the relatively high rate constant of reverse reaction R3 under high
7 temperature. So, in the following discussion of elementary reactions, we only consider the positive
8 reactions. For R9 and R13, the positive reaction rates show exponential decay with increasing
9 temperature. On the other hand, the mole fractions of H and OH are increased in moderate-
10 temperature regions for Case $\varphi = 0.6$. As a result, the heat release is enhanced in moderate
11 temperatures for Case $\varphi = 0.6$ in Fig. 10. For reaction 3, the positive reaction rate and OH mole
12 fraction all experience exponential growth with increasing temperature, which is more significant
13 under higher equivalence ratio. These dual effects promote the reaction of R3 under high φ , which
14 explains why R3 overtakes R13 as the second most dominating reaction for Case $\varphi = 0.6$. It is also
15 noted in Fig. 10 that R8 is enhanced in high-temperature regions under high φ . This could possibly
16 be attributed to the high contribution of H₂O to third-body [M] in Eq. 3. When the equivalence ratio
17 is increased, the H₂O concentration under high temperatures is also increased, which will contribute
18 to a high [M] value. For R11, the positive rate constant levels off after 1000 K. Thus, although the
19 HRR of R11 is increased, the difference between moderate-temperature and high-temperature regions
20 is not as evident as other reactions.

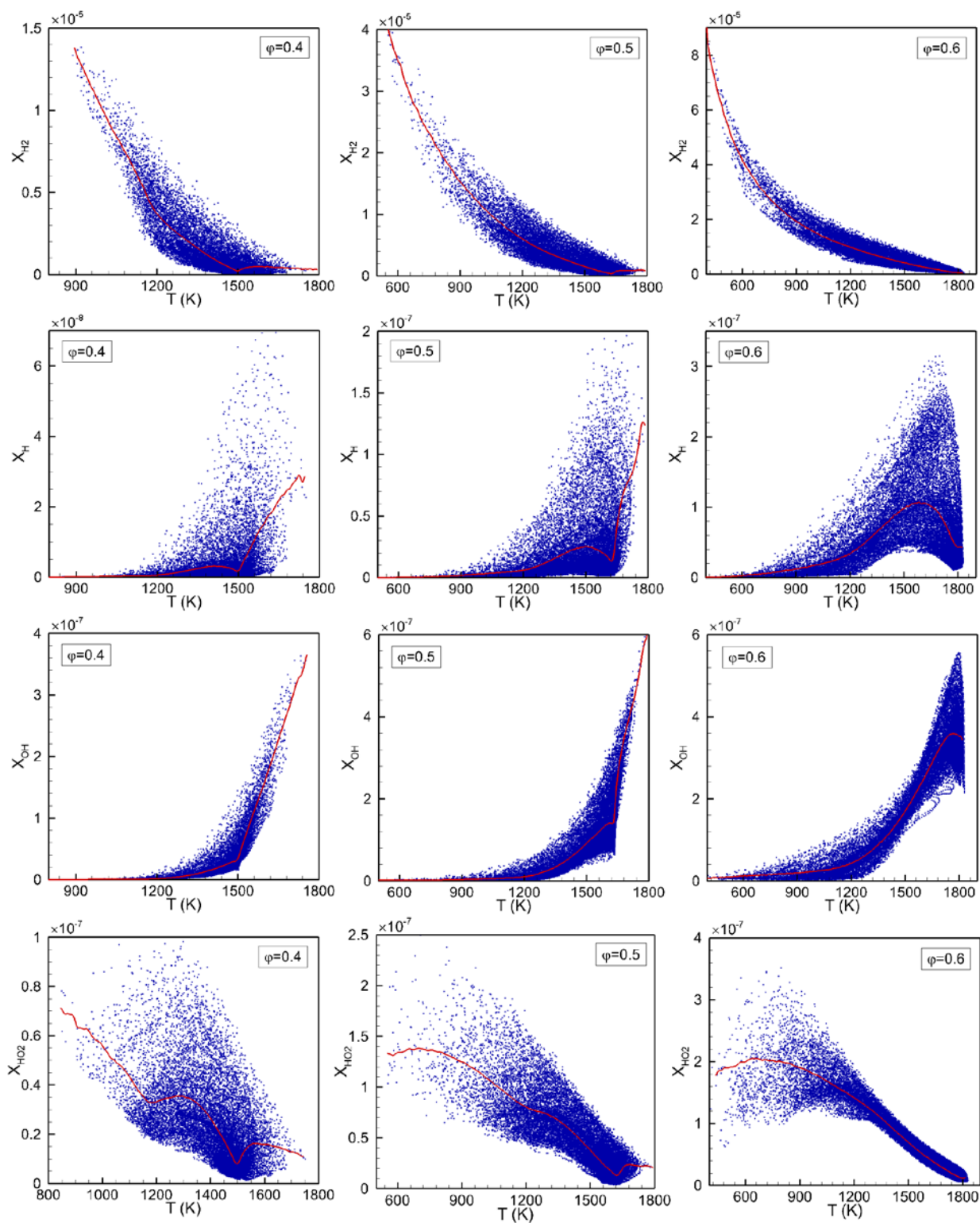


Fig. 11 - Scatter plots of main species mole fractions in the reaction zone. The solid red lines denote the mean values conditioned on temperature.

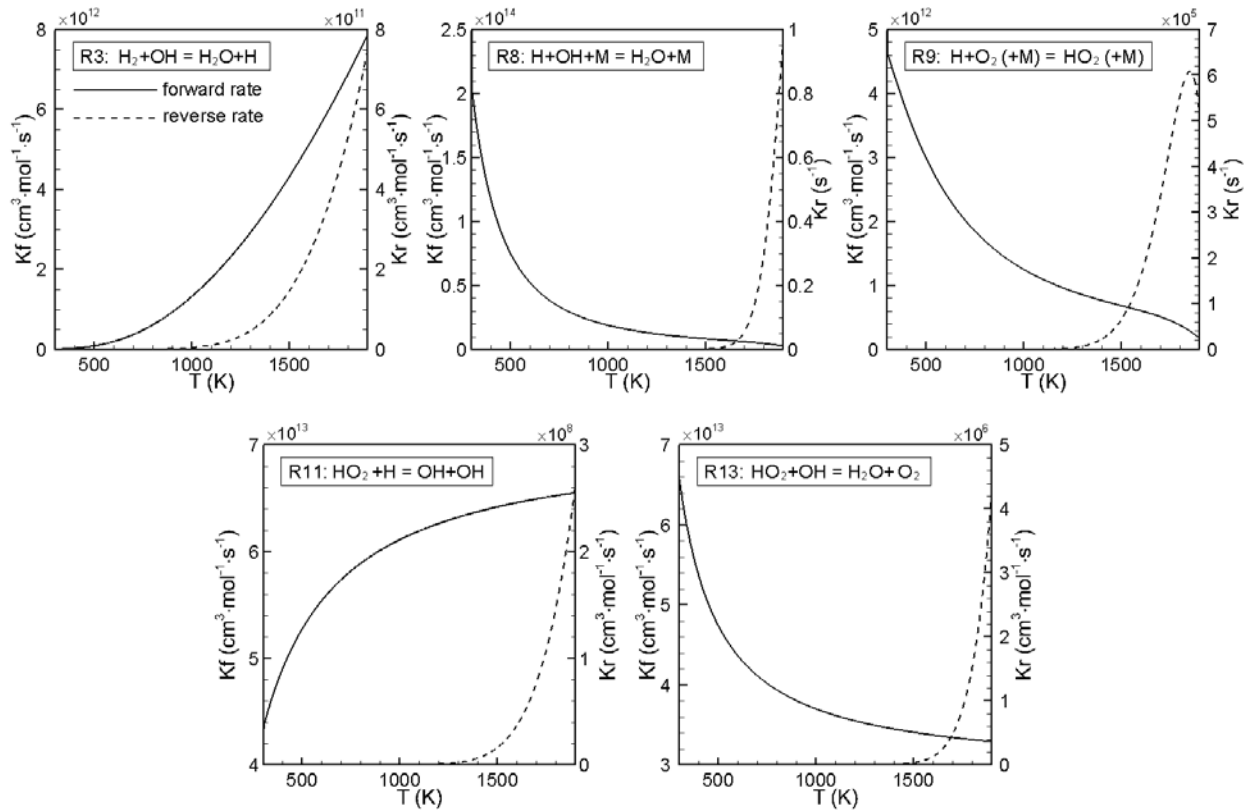


Fig. 12 - Forward and reverse reaction rate constants versus temperature for the main heat release reactions.

The solid lines denote the forward reaction rate and the dashed lines denote the reverse reaction rate.

4. Conclusions

In this study, three-dimensional direct numerical simulations of H_2 /air flames are carried out to investigate the characteristics of heat release under various equivalence ratios. These flames are simulated at high Karlovitz number and high pressures which are relevant to lean-burn gas turbine conditions. Reaction zone structures, local equivalence ratio, flame front curvature and elementary reaction rates are examined statistically with the objective of extending our understanding of lean combustion under high-pressure conditions.

Under different lean conditions ($\phi = 0.4, 0.5, 0.6$), the turbulent flame fronts show similar topological structures for the three cases under the same Karlovitz number, even though the higher ϕ case is characterized with stronger heat release rate. It is also noted that the relative thickness of reaction zone (δ_f / δ_L) is increasing for both laminar and turbulent flames with increasing equivalence ratio. However, the extent of increase for heat release and reaction layer thickness is reduced under

1 high ϕ , which indicates that turbulent transport is overtaking differential diffusion as the main effect
2 on the high Ka flames.

3 The turbulent flames behave differently in positive and negative curvature regions. It is observed
4 that the trenches of local equivalence ratio ϕ_L are located at concave structures inside the reaction
5 zone, while ϕ_L plateaus are situated at convex structures outside the reaction zone. With increasing
6 equivalence ratio, the trench ‘depth’ and plateau ‘height’ are reduced, which is primarily due to the
7 decreased Lewis number. In addition, ϕ_L is found to be significantly higher than mixture ϕ under
8 ultra-lean conditions, resulting in hot spots in the reaction zone. This finding suggests that the benefits
9 of lean combustion in terms of lowering peak flame temperature and reducing NO_x emission may
10 be slightly cut down under ultra-lean conditions, which is instructive for industrial applications.
11 Furthermore, the temperature iso-surfaces show that the enhancement (weakening) of heat release in
12 convex (concave) regions is reduced as ϕ is increased in the reaction zone.

13 The heat release behaviour in the reaction zone is explained by analysing radical distribution and
14 rate constant as a function of temperature. At high equivalence ratio, the radical transportation and
15 concentration are significantly increased. The high radical fractions in regions with over-adiabatic
16 temperature contribute to the formation of hot spots directly under ultra-lean conditions. As the rate
17 constants of reaction $\text{H} + \text{O}_2 (+\text{M}) = \text{HO}_2 (+\text{M})$ and $\text{HO}_2 + \text{OH} = \text{H}_2\text{O} + \text{O}_2$ decay exponentially with
18 increasing temperature, their heat releases are relatively enhanced in moderate-temperature regions,
19 which contributes to a broadened reaction zone for the case with higher equivalence ratio. In summary,
20 due to the combined effects of radical fractions and reaction rate constants, the local heat release is
21 changed in different temperature windows when the mixture equivalence ratio varies.

22

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