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Microstructure of fibres pressure-spun from polyacrylonitrile – graphene

oxide composite mixtures

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Abstract

Suspensions containing 8 and 10 wt% polyacrylonitrile (PAN) and 1, 2, 3, 5, 7 and 10 wt% graphene oxide (GO) were prepared using a special mixing routine and fibres were generated from these mixtures by pressurised gyration. The combination of pressure and gyration speed was effective in controlling the fibre morphology and fibre diameter which ranged from $1 - 20 \mu m$. Fibres were pyrolyzed to remove the polymer and only the 10 wt% PAN fibres survived. The microstructure of the pre- and post-pyrolysis products were characterised by scanning electron microscopy, both with and without focussed ion beam etching, Fourier-transformed infrared and Raman spectroscopies. Pyrolyzed fibre electrical conductivities were measured and only those containing 1 and 2 wt% GO were conductive.

1. Introduction

In recent years, there has been an increasing interest in graphene; as the specific surface area of graphene sheets is high owing to their single-layer morphology and two-dimensional nature. Graphene-based fibres have superior mechanical properties^{1–6}. Reduced GO (rGO) fibres have recently been reported to be electrically and thermally conductive⁷, durable, flexible, and chemically resistant⁸. The potential applications of rGO fibres are in multifunctional textiles, wearable electronics, fuel cell, battery, sensor and filters^{9–14}. GO made by oxidation of graphite, a cheap and abundant material compared to expensive single-layer graphene. It is easy to process since it is dispersible in water (and other solvents), and it is used to make graphene.

Fabrication of graphene or GO fibres can be carried out by wet-spinning¹⁵, laser reduction¹⁶, coagulation^{17–21} and pressurised gyration^{22,23}. Most of these studies focused on the effects of wet-spinning, coagulation and reduction conditions. Uniform natural and synthetic polymer nanofibres could be mass-produced using simple one-step pressurised gyration more consistently, robustly and reliably at low cost compared to wet-spinning and electrospinning techniques. The successful dispersion of GO in suspension, on the performance of the obtained graphene fibres and application in energy storage devices, have been studied in detail²⁴. The focus of this paper is to use the pressurised gyration for making GO-loaded fibres and products derived from them, a topic that has not been studied in detail.

Graphene precursors such as graphite sulphate and polyacrylonitrile (PAN) have enabled studies of graphene fibres. A precursor is a compound that participates in a chemical reaction that produces another compound, in this case, graphene. PAN has been extensively studied

for making carbon nanofibres because of its advantages of having a high carbon yield, compared with other polymers, and being relatively inexpensive^{8–10}. Graphite sulphate was used as a precursor by Eigler²⁵ however, the functionality was not proven with lower yields of graphene. Meanwhile, PAN, a form of acrylic fibre, is the predominant precursor material for the production of carbon fibres. The quality and composition of PAN precursors determine the ultimate performance of carbon fibres. A series of thermal treatments must be carried out to convert the PAN fibres to high tenacity carbon fibres, including thermal stabilization (~300 °C), carbonization (~1000 °C) and graphitization (>2000 °C)²⁶. PAN is desirable as a carbon precursor because of its higher melting point and greater carbon yield compared with pitch and rayon, the natural precursors. Some of the key challenges using natural precursors, which need further processing and purifying to form fibres, are that it is very expensive compared to PAN-based fibres²⁷.

The use of pristine graphene in the development of graphene-based polymer composites is limited, owing to its high specific surface area and strong intermolecular interactions between graphene sheets which in turn limits the improvement in the properties of composites. Also, the electrical properties of graphene-polymer composites typically depend on electron percolation between independent filler particles. Hence, an excellent dispersion of graphene is important to produce a conductive polymer matrix.

Pressurised gyration, which involves high-speed rotation of a perforated pot containing a polymer solution, is a promising alternative method of spinning fibres and fibrous structures^{28,29}. The high production rate (up to 6kghr⁻¹), ease of processing and highly controlled fibre morphology are salient features of this technique²⁸. In this work, the effects of process parameters on the properties of GO fibre such as fibre morphology and roughness,

crystalline structure have been analysed in detail by scanning electron microscopy (SEM), Fourier-transform infrared spectroscopy (FTIR), Atomic force microscopy (AFM) and Raman spectroscopy (Raman). Also, PAN-GO composite fibres were prepared to investigate the effects of composition, speed and pressure on the structural morphology of the fibres. Some of the fibres were subjected to controlled pyrolysis after which electrical conductivity of the fibres was tested. The relationship between the processing parameters and the structural features of GO fibre are discussed in detail in this work.

2. Experimental Details

2.1 Materials

Polyacrylonitrile (average molecular weight 150,000), and N, N-dimethylformamide (DMF) was purchased from Sigma Aldrich (St. Louis, MO, USA) and used as received without further purification. The GO used in this study was synthesised according to a modified Hummer's method³⁰ at the University of Sheffield, UK. The process is reproducible and GO particles were 2-3 μ m diameter (Figure S1(d)).

2.2 Preparation of graphene oxide (GO) suspensions

The preparation of GO suspensions and polymer solutions containing GO are detailed in **Supplementary Information S1**. The detailed experimental procedures are also given in **Supplementary Information S2**.

2.3 Characterisation

Details of characterisation of polymer solutions and the resulting products, in this case, composite fibres are given in **Supplementary Information S3**.

3. Results and discussion

Figure 1 shows that at the lowest rotational speed of 10k rpm in the 8 wt% polymer composition, none of the compositions led to fibres, producing a polymeric spray instead. It is because the critical minimum rotation speed has not been exceeded, and it is too slow for a solution to move to the orifice and thus no polymer was accelerated to carry the GO particles and for the subsequent jetting to form fibres.



Figure 1 Diameter of fibres spun from 8 wt% PAN at different speeds and pressures

On increasing the speed to 24k rpm, all of the solutions formed fibre composites as the centrifugal force exceeded the surface tension percolation threshold of the polymeric solutions, creating a polymer jet which subsequently leaves behind a bundle of fibres. These refer to fibre layer length (circumferential) that could be varied from 0.3-0.8 meters and

each layer consists up to 100 fibres. At 3 wt% GO fibre is the thinnest and most uniform in diameter. However, increasing the speed to 36k rpm, only 5 wt% and 7 wt% GO formed randomly orientated fibres. This is likely to be due to the sliding of GO sheets when the rotation speed was exceeded.

Increasing pressure to 0.2 MPa with a rotational speed of 10k rpm allowed the preparation of smaller fibres, 3 wt% GO compared to 10 wt% has a much smaller diameter fibre (**Figure 1**) and is more uniform. With a higher percentage of GO, 7 wt% and 10 wt%, the aggregation of GO might cause less sliding because steric hindrance at the surface of the GO sheets inhibits stacking, and stable dispersion inhibits agglomeration. This effect may cause a reduction in surface tension and increased viscosity and polymer entanglement. The 8 wt% PAN-based fibres had a mean diameter of 7.3 μ m. The fibre diameter hence shows a gradual decrease in GO content, but the size distributions also broaden. Similar trends are seen with 10 wt% PAN which has a mean diameter of 6.2 μ m.

The external driving force is the gravitational force when a polymer drop emerges from the orifices²⁸ because surface tension inclined along the liquid-air interface separates the drop from the surrounding air. Fibre formation from this process starts with a jet emerging from the orifice on the face of the vessel. The jet further stretches due to the centrifugal force and the pressure difference at the orifice. Finally, the evaporation of the solvent leads to thinning of the fibres. The reason for only jet formation instead of droplets in this surface instability is viscoelasticity of the polymer solution used²⁸. Thus, most of the solutions did not produce fibres at 3 wt% GO 8 wt% PAN.

Figure 2 shows the fibres formed when the speed is 24k rpm and 36k rpm at all concentrations and pressures. Composition of 10 wt% GO shows the highest fibre diameter considering all process variables, due to more GO particles in the fibres. For the 10 wt% PAN-GO fibres, at the lowest rotational speed of 10k rpm and at 0.1 MPa pressure, none of the compositions formed fibres, except 7GO and 10GO. Increasing the speed to 24k rpm caused all the suspensions to form composite fibres. However, on increasing the speed to 36k rpm, all compositions formed fibres. At a pressure of 0.2 MPa with a rotational speed of 10k rpm, 3 wt% GO didn't yield any fibre but all other compositions did. Increasing the rotating speeds to 24k and 36k rpm, caused fibres to form because they reach the stability of the polymer viscoelasticity.



Figure 2 Diameter of fibres spun from 10 wt% PAN at different speeds and pressures

Generally, fibre diameter is large for 24k rpm compared to 36k rpm. At a pressure of 0.3 MPa with 10k rpm rotating speed, all the compositions produced fibres except 10GO. By increasing the rotating speeds to 24k and 36k rpm fibres were formed. Generally, fibre diameter didn't show any variation for 24k rpm and 36k rpm for all compositions, exclude

10GO. It is well known that the centrifugal force applied to the polymer solution is the driving force for the jet formation and mostly affected by the rotating speed. It further influences the exit velocity of the jet, the jet's path to the collector and thus fibre diameter and the fibre morphology. The increase of rotational speed accelerates the polymer chain elongation, thus improving jet attenuation and the fibre diameter decreases.

However, the solution mass throughput from the nozzle not only depends on the rotating speed but is also governed by pressure difference at the orifice. On the other hand, rotating speed influences the airflow that acts outside of the spinneret and helps the evaporation of the solvent. Higher airflow accelerates solvent evaporation, which suppresses the elongation of the polymer jet resulting in thicker fibres. This may be the reason for the variation in the fibre diameters with various pressures in the process. **Figure 3** shows the fibre diameter distribution for different polymer systems.



Figure 3 Diameter distribution of the 7GO 10PAN for different speeds and pressures.

In the 7 GO - PAN polymer system, the mean diameter is $4.2 \pm 1.6 \,\mu\text{m}$ at speed of 10k rpm and 0.1 MPa. Increasing the speed to 24k rpm, mean diameter reduced to 1.0 ± 0.62 and increase to 3.4 ± 0.64 when the speed increased to 36k rpm. However, at a pressure of 0.2 MPa and 0.3, mean diameter decreased when the speed is increased. At the speed of 10k rpm and pressure of 0.2 MPa, the mean diameter is 4.5 ± 2.14 , then 3.7 ± 0.85 at 24k rpm and reduced to 3.2 ± 0.95 . Similarly, for the pressure of 0.3 MPa, at a speed of 10k rpm, the mean diameter is 4.4 ± 1.45 then 4.3 ± 0.62 and reduced to 3.7 ± 0.84 at the speed of 36k rpm.

SEM images of spun fibres using 3, 5, 7 and 10 wt% solutions and subjected to 10k - 36k rpm and $1 - 3 \times 10^5$ Pa is shown in **Figures 4** and **5**. The mean fibre size ranged from 1 - 20 µm for the 3 - 10 wt% solutions. At fixed (1×10^5 Pa) pressure and 36k rpm rotational speed a trend of increasing average fibre size is shown when the percentage of GO is increased.

This is attributed to the volume and mass of polymer solution that is being transferred across the orifice. Thicker polymer jets were formed at a higher polymer and GO concentration which, on the other hand, hinders the evaporation of the solution, causing a more significant transfer rate of the solution across the vessel orifices.

Fibre formation started at a lower concentration for 3GO 10PAN spun at 10k rpm at a pressure of 0.3 MPa (**Figure 4a**). However, the speed was not enough to complete the process and jet out only fibres and polymeric lumps containing GO were found in the product. The increase in pressure from 0.1 to 0.3 MPa is not sufficient to compensate for low speed.



Figure 4 (a) Fibres started to form in 3GO 10PAN, 10k rpm at 0.3 MPa (b) 24k rpm 0.1MPa and (c) 24k 0.2 MPa

Figures 4 (b) and **(c)** shows that by increasing pressure, the PAN-GO solution is thinned and the disjoining pressure affects the capillary interactions between particles attached to the fibre surfaces. It appears that particles are protruding from a solution and that capillary rise of the liquid occurs along the surface of each particle³¹.

Figure 5 shows that at a speed of 36k rpm and pressure of 3×10^5 Pa, in composition 3GO 10PAN fibres formed, in particular, **Figure 5(b)** shows that a graphene composite fibre knot can be stretched under tensile stress, leading to the high fracture elongation of the graphene fibre¹⁵.



Figure 5 3GO 10PAN fibres obtained at 36k rpm with pressure at (a) 0.2 MPa and b) 0.3 MPa

The influence of pressure applied during gyration in generating different fibre morphologies was studied by fixing the rotational speed at 36k rpm and conducting experiments at 1×10^5 , 2×10^5 , and 3×10^5 Pa for 3-10 wt% solutions. It is evident that, in general, a narrow

diameter distribution of fibre diameter is achieved at higher working pressures (Figure 6).

At any fixed polymer concentration, by increasing the pressure, a trend of reduction in the fibre diameter was observed. This is due to the introduced gas stream which enhances the combined shearing force (consisting of centrifugal force and blowing) against the surface tension force in the elongational flow of polymer jets²⁸. Therefore the diameters of the ejected polymer jets at the orifices of the vessel were reduced, which helps to promote thinner fibre formation. Solvent evaporation can be enhanced by blowing a hot air gun which affects the relative speed of airflow on the liquid-air interface in the polymer at the fibre surface, thus contributing to fibre formation. Reducing humidity to a range of 35 - 42% RH also promotes fibre formation.

0.1 MPa

0.2 MPa

0.3 MPa



Figure 6 Scanning electron micrographs of 7GO 10PAN fibres produced at different pressures and speeds

Initially, a jet emerges from the orifice on the face of the vessel. This jet further stretches due to the centrifugal force and the pressure difference at the orifice. Finally, the evaporation of the solvent leads to thinning of the fibers formed²⁸. There was a strong relationship between the magnitude of pressure applied and the speed at which the solution escaped from the orifices, which led to improved fiber morphology. The morphology of fibers, homogeneity of fiber distribution, and production yield improved by increasing the spinning speed but was further enhanced by increasing the gas pressure³².

These results also indicate that the polymer concentration has a significant influence on the as-spun fibre morphology, that is, the increased polymer viscosity plays a role of stabilising polymer jets against the action of centrifugal force and dynamic solution blowing, hence promoting larger fibre diameter. When the polymer concentration is continuously increased, solvent evaporation is hindered. Hence it leads to the relatively long relaxation time/evaporation time during stretching. If the concentration of polymer is too low, only droplets or beads were formed or the creation of bead on string fibres was promoted. Higher molecular weight resulted in higher viscosity and a higher number of chain entanglements which means thicker fibres will be produced.

A minimum rotation speed that could result in enough viscous solution response enables the generation of nanofibres at lower polymer concentrations. On the whole, increasing rotational speed accelerates stretching of polymer jets, this decreases the diameters of the polymer jets at the orifices of the vessel, and thinner fibres are obtained. It is seen that, overall, narrower size distribution is obtained at a higher rotational speed. It is noteworthy that at 10k rpm, not

all the solutions are spinnable using a typical pressurised gyration method at a pressure of 1×10^5 Pa using 8 wt% PAN.

It is a significant challenge to directly assemble 2D GO sheets into 1D fibres without any polymer or surfactant, due to the lack of scalable assembly methods³³, the size and irregular shape of chemically derived graphenes and the movable layer-by-layer stacking of graphenes³⁴. Therefore, in order to integrate the remarkable properties of individual graphene sheets or its derivatives into advanced, macroscopic, and functional structures for practical applications, an effective assembly strategy in a well-controlled way has to be developed¹⁹. And this work paves the way for that.

3.1 Fibre chemistry

Polymer compatibility is a crucial factor in determining the stability of fibres. If the GO is not compatible with PAN polymer, then a solid phase separation will be observed. Secondary interactions such as hydrogen bonding, hydrophobic reactions, and electrostatic forces can increase the compatibility in the fibres³⁵. FTIR spectroscopy has been used to reveal the bonding profile of composite, GO and PAN. FTIR spectra of GO, PAN and PAN-GO are represented in **Figure 7**. The FTIR spectrum of GO shows characteristic bands at 3500 cm⁻¹ (C-H stress) and 1500 cm⁻¹ (C=O stress), while the spectrum of GO-PAN contains peaks at 2448 cm⁻¹ (N-H stretching, aromatic and aliphatic C-H stretching). The frequency of the physical mixture is a composite of the pure polymer, containing all the characteristic bands of GO-PAN. This indicates that the interactions between GO and the polymer are weak when they are mixed physically.



Figure 7 FTIR of GO, PAN and GO-PAN

The FTIR spectrum of PAN displays characteristic bands of methyl and methylene C-H stretching vibrations at 3000 cm⁻¹ and 1560 cm⁻¹ respectively, as well as a strong band due to carbonyl groups at 1500 cm⁻¹ (C=O stretch) and two bands due to ester linkages (C-O-C stretches). Therefore, it suggests there is good compatibility between GO and PAN. Another peak for PAN fibres is observed in the range of 2243-2246 cm⁻¹ which is related to the presence of nitrile (C=N) bonds, indicating that the nitrile group exists in the PAN chain. The broad signal between 3200 cm⁻¹ and 3700 cm⁻¹ is generated from O–H stretching vibration and adsorbed water molecules. Two peaks at 2925 cm⁻¹ and 2855 cm⁻¹ are assigned to asymmetric and symmetric vibrations of CH₂ groups, respectively. The strong signal at 1738 cm⁻¹ in the GO's spectrum refers to the C=O stretching vibration which was significantly weakened after reduction. The peak at 1622 cm⁻¹ is attributed to the C=C stretching vibration. There are carbonyl stretching regions (1681-1764 cm⁻¹), CH₂ deformations (1380-1500 cm⁻¹), and aromatic stretches from the hard segment (1617 cm⁻¹), and amide II mixed band (1540 cm⁻¹).

Raman spectroscopy is widely used to characterise crystal structure, disorder and defects in graphene-based materials. Structural changes during the oxidation and reduction processes were monitored by Raman spectroscopy. Raman spectra of GO are characterised by the changes in the relative intensity of two main peaks: D and G. Raman scattering systems were also used to evaluate the hybridisation of the state in carbon, and the two reflection peaks change from pristine graphite to its derivatives. As shown in Figure 8a, a strong band at 1600 cm⁻¹ (G band) and a relatively weak band at 1352 cm⁻¹ (D band) appear in the Raman spectra of pristine graphite, which stem from the vibration of the sp²-hybridised graphitic domain, and sp³-hybridized carbon or structural defects, respectively. The low I_D/I_G value (0.20) indicates the graphitic domains is primarily intact for pristine graphite. It was mainly induced by the n-type effect on the GO which forms the sp^2 carbon modification to sp^3 which is why the intensity ratio of D band and G bands decreased. Comparing the Raman spectra before and after pyrolysis (see Section 3.2), it has been revealed that there has been a clear change of crystal structure from pristine GO to GO-composite, indicating the reduction of GO into graphene (reduced graphene). The reduction of functional groups onto the surface of GO was also verified by the decrease in intensity of GO after pyrolysis (Figure 8b).

It was observed in **Figure 8b** that there is a broad Raman peak centred at 1552 cm⁻¹. The broadness of the Raman band suggests that PAN fibres represent disordered arrangements of PAN molecules. The sharpness of this peak was observed with increasing concentration of GO in the composite revealing the ordered arrangement of GO within composites. Two characteristic peaks at 1340 and 1552 cm⁻¹ were observed in composites. These peaks correspond to the D and G bands from the defect structure of sp³-carbon and the plane vibration of the sp²-carbon atoms in a two-dimensional lattice of the GO-PAN composite^{36,37}.

Raman spectral signatures confirm that the cyclization of PAN is associated with graphitization. This feature was observed in all the spun fibres (**Figure 8**).



Figure 8 Raman spectroscopy of (a) as spun GO PAN solutions and (b) pyrolysed 10GO 1 and 2 wt% PAN

3.2 Pyrolysed fibres

To achieve optimal graphene fibre properties, a heating rate of 1 °C/min and a treatment time of 30 min was used. After carbonization to 900 °C, graphene fibres were obtained. A PAN-based precursor containing carboxylic acid groups and acrylamide units was used for increasing the stabilization rate and sulphate/sulfonic groups for controlling the denseness of the precursor fibres³⁸. Residues from the spinning solution can also behave as an initiator for nucleophilic cyclization reactions to reduce stabilization time³⁹.

The fibre diameter was reduced with the removal of the non-carbon elements. At the early stages of carbonization, crosslinking reactions take place in the oxidized PAN. The cyclized structure starts to link up in the lateral direction by dehydration and denitrogenation. A planar structure can be formed with the basal planes oriented along the fibre axis.

By increasing GO, the surface of the fibres became rougher and up to 3 wt% GO (**Figure S2d**), the fibres started to break. This supports the observation on electrical conductivity where only up to 2 wt% was significant. This might be due to the graphene fibres becoming brittle due to a high percentage of carbon caused by including PAN as a carbon precursor, which forms carbon during pyrolysis.

These fibres are generally called "high strength" fibres³⁹. The strength of carbon fibre is observed to increase with the carbonization temperature and the maximum strength is observed at around 1500 °C. Too fast carbonization introduces defects in carbon fibres, while a low carbonization rate causes the loss of too much nitrogen at the early stages of carbonization³⁹.



а



Figure 9. Scanning electron micrographs of focussed ion beam etched samples (a) control (b) prepared fibres

To verify the presence of graphene in the pyrolysed fibres, focussed ion beam cross-section studies were carried out (**Figure 9**). For the control sample, 10% PAN fibres (without GO) were pyrolysed. Before SEM and FIB, a 15 nm coating of platinum (45s of sputtering was deposited). Pyrolysed 3wt% GO - 10wt% PAN fibres (**Figure 9**) show distinct grainy internal morphology, whereas the control (**Figure 9a**), pyrolysed 10wt% PAN fibres show a smooth, porous internal structure.

3.3 Electrical conductivity

b

Figure 10 shows that a LED illuminates when connected to pyrolyzed fibres. However, only 1 wt% GO 10 wt% PAN and 2 wt% GO 10 wt% PAN with values of 973 S/m and 459 S/m

respectively shared this phenomenon. There was no electrical conductivity in the as-spun fibres as the insulating behaviour of GO dominates. Even post-pyrolysis, at high percentages of GO, there is no conductivity because it became dependent on geometrical aspects like sheet orientation and percolation effects in the fibre, causing the gross diversity⁴⁰. This situation complicates any prediction of the conductivities for GO composite material formulations and affects the reliability of any theoretical model or simulation⁴¹. Guex et. al⁴⁰ suggested this was caused by the preferential attack of reducing agent on C-O rather than C=O groups. This is confirmed by the fact that the G band stronger at 1 wt% GO than 2 wt% GO (**Figure 8**).



Figure 10 Electrical testing, inset shows the circuitry

4.0 Conclusions

Different GO-PAN compositions were processed using pressurised gyration to obtain fibrous products. The processing parameters such as rotating speed, working pressure and the concentration of GO-polymer composite solution had a significant influence the fibres formed. Generally lower concentration of GO and the higher rotating speed of 36k rpm resulted in small fibre diameter. The fine fibres were also obtained by increasing the working pressure from 0.1 MPa to 0.3 MPa. The fibre diameter distribution was unimodal for all the processing conditions and the mean diameter ranged from 1-20 μ m. The SEM and FIB

imaging showed that GO platelets were incorporated in the fibres. The findings also revealed that fibre morphology was dependent on GO concentration. It was shown at 10 wt% PAN compared to lower concentrations of 8 wt%, generated more fibres even at lower pressure and speed. Pyrolysed fibres showed granular morphology while the controlled sample without GO had a smooth surface. FTIR and Raman spectroscopy showed the characteristics of bonding existed in the polymer and GO. Fibres were successfully pyrolyzed, however, only lower loading of GO with 10 wt% PAN (1 - 2 wt%), had conductivity.

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Declaration of interests

☑ The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

The authors declare the following financial interests/personal relationships which may be considered as potential competing interests:

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